

# Remediation of oil-contaminated harbor sediments by chemical oxidation

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2	Remediation of oil-contaminated harbor sediments by chemical oxidation
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#### 24 Abstract

25 Oil hydrocarbons are widespread pollutants in sub-surface sediments with serious threats to terrestrial and aquatic environment. However, very limited data is available about 26 27 remediation of historically contaminated sediments. This study reports the use of magnetite-28 catalyzed chemical oxidation (H<sub>2</sub>O<sub>2</sub> and Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>) to degrade oil hydrocarbons in aged 29 contaminated sediments. For this purpose, oil contaminated sediments were sampled from 30 three different locations in France including two harbors and one petroleum industrial 31 channel. These sediments were characterized by different hydrocarbon index (HI) values (3.7 -9.0 g kg<sup>-1</sup>), total organic carbon contents (1.9% -8.4%) and textures (sand, slit loam and 32 33 silt). Chemical oxidation was performed in batch system for one week at circumneutral pH 34 by: H<sub>2</sub>O<sub>2</sub> alone, H<sub>2</sub>O<sub>2</sub>/Fe(II), H<sub>2</sub>O<sub>2</sub>/magnetite, Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub> alone, Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/Fe(II), and 35 Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/magnetite. Results obtained by GC-FID indicated substantial hydrocarbon 36 degradation (40 – 70%) by  $H_2O_2$ /magnetite and  $Na_2S_2O_8$ /magnetite. However, oxidants alone 37 or with soluble Fe(II) caused small degradation (< 5%). In the presence of  $H_2O_2/magnetite$ , 38 degradation of extractable organic matter and that of HI were highly correlated. However, no 39 such correlation was observed for Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/magnetite which resulted in higher removal of HI 40 indicating its selective oxidation behavior. Treatment efficiency was negatively influenced by 41 organic carbon and carbonate contents. For being the first study to report chemical oxidation 42 of oil hydrocarbons in real contaminated sediments, it may have practical implications to 43 design a remediation strategy for target contaminants.

44

45 Keywords: Oil hydrocarbons; Harbor sediments; Remediation; Fenton-like; Persulfate;
46 Magnetite

#### 48 **1. Introduction**

49 Oil hydrocarbons are widespread pollutants in sub-surface sediments which pose serious 50 threats to terrestrial and aquatic environment. Therefore, development of novel and effective 51 remediation techniques for oil-contaminated sediments is of considerable environmental 52 interest (Lim et al., 2016). Various remediation techniques have been developed including 53 biological (Chaîneau et al., 2003; Benyahia et al., 2005), chemical (Usman et al., 2012a; 54 2013; Chen et al., 2016) and combined approaches (Silva-Castro et al., 2013; Souza et al., 2014; Agarwal and Liu, 2015; Xu et al., 2016a). Bioremediation is the most commonly used 55 56 technique to remediate oil contaminated matrices (soils, sediments and water) primarily 57 because of its cost-effective and environment friendly nature (Lim et al., 2016). Majority of 58 molecules in crude oil spills and refined products are biodegradable and thus can largely be 59 removed by bioremediation (Prince, 1993). However, bioremediation often leaves non-60 biodegradable residues due to incomplete mineralization and thus cannot meet the stringent 61 environmental cleanup standards reported by environmental regulations (Płaza et al., 2005). 62 Contamination level had reached a plateau for long time in soil subjected to bioremediation 63 for two years (Lu et al., 2010). Bioremediation or natural attenuation of n-alkanes present in oil lead to their degradation whereby leaving unresolved complex mixture (UCM) composed 64 65 of iso- and cyclo-alkanes, which is totally refractory to microbial attack (Chaillan et al., 2006; 66 Farrington and Quinn, 2015). However, chemical oxidation has shown strong efficiency to 67 remove oil hydrocarbons where different oxidants are used to degrade organic pollutants. 68 Recent studies employing chemical oxidation for the remediation of oil hydrocarbons are 69 summarized in Table 1. Among chemical oxidation-based treatments, Fenton and persulfate 70 oxidation are showing great remediation potential to remove oil hydrocarbons. Both oxidants 71 require ferrous iron Fe(II) to produce stronger radicals through following reactions:

72  $\operatorname{Fe}(\operatorname{II}) + \operatorname{H}_2\operatorname{O}_2 \longrightarrow \operatorname{Fe}(\operatorname{III}) + \operatorname{HO}^- + \operatorname{HO}^{\bullet}$  (1)

73 
$$S_2O_8^{2-} + Fe(II) \rightarrow SO_4^{-} + SO_4^{2-} + Fe(III)$$
 (2)

74 Activation by soluble Fe(II) requires an acidic pH (~ 3) to avoid its precipitation which is 75 harmful for soil quality and microbial population (Laurent et al., 2012). This initial 76 acidification can be avoided by using chelating agents or iron minerals to perform chemical oxidation at circumneutral pH (Usman et al., 2016b). Iron oxides especially mixed-valent 77 78 Fe(II)-Fe(III) minerals like magnetite [Fe(II)Fe(III)<sub>2</sub>O<sub>4</sub>] and green rust were found more 79 effective to catalyze chemical oxidation as compared to the ferric minerals or soluble Fe(II) at circumneutral pH due to the presence of structural Fe(II) (Usman et al., 2018). Previous 80 81 batch (Usman et al., 2012a) and column experiments (Usman et al., 2013) showed that 82 magnetite-catalyzed chemical oxidation (Fenton-like and persulfate) is highly efficient to 83 remove oil hydrocarbons (90% degradation) in crude oil as well its refractory product after 84 biodegradation (UCM). However, these findings were based on artificially contaminated sand where oil hydrocarbons were spiked on sand after extraction from contaminated sediments. 85 86 To date, no study has been published on use of chemical oxidation to remediate real oil-87 contaminated sediments. It should be noted that chemical oxidation resulted in significant 88 removal (80%) of polycyclic aromatic hydrocarbons (PAHs) when extracted from aged contaminated soils and spiked in sand. However, these treatments were ineffective (<5% 89 90 degradation) in aged contaminated soils (without any extraction) which has been attributed to 91 the contaminant unavailability (Usman et al., 2012b; 2012c; 2016a; Biache et al., 2015). In 92 the present study, we aim to evaluate the efficiency of hydrogen peroxide  $(H_2O_2)$  and 93 persulfate (Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>) catalyzed by magnetite to remove oil hydrocarbons in aged 94 contaminated sediments. Remediation of three kinds of sediments sampled from different 95 locations in France were investigated. These sediments were subjected to magnetite-catalyzed 96 chemical oxidation at circumneutral pH under different conditions (H<sub>2</sub>O<sub>2</sub> or Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub> with or 97 without Fe(II) or magnetite as catalyst). Organic analyses were performed by using Gas 98 Chromatography - flame ionization detector (GC-FID). The performance of chemical 99 oxidation treatment in correlation with the availability of oil hydrocarbons in aged 100 contaminated sediments was discussed.

Oxidant	Catalyst type	Target pollutant and its initial concentration	Medium	Experimental conditions	Extent / rate of pollutant degradation	Ref.
H <sub>2</sub> O <sub>2</sub>	Magnetite (Commercial) Screened through 0.3 mm sieve.	Petroleum hydrocarbons 1 g Kg <sup>-1</sup>	Spiked sand/ Batch			(Kong et al., 1998)
H <sub>2</sub> O <sub>2</sub>	Soluble Fe(II)	Diesel 10-12 g Kg <sup>-1</sup>	Spiked sand and peat soil/ Batch	pH = 3, H <sub>2</sub> O <sub>2</sub> :Fe(II) molar ratio = 10:1 liquid/solid = 1 and 20 mL $g^{-1}$ for sand and peat		(Goi et al., 2006)
H <sub>2</sub> O <sub>2</sub>	Basic oxygen furnace slag	Fuel oil or diesel TPH = 10 g kg <sup>-1</sup>	Spiked sand and sandy Ioam/ Batch	pH = 6.7, $H_2O_2 = 15\%$ $Slag = 100 g kg^{-1}$	TPH removal of 96% and 76% in diesel and fuel oil tests after 40 h	(Tsai and Kao, 2009)
H <sub>2</sub> O <sub>2</sub>	Soluble Fe(II) in the presence or absence of natural soil Fe minerals (hematite mainly)	Diesel 5 g Kg <sup>-1</sup>	Spiked loam soil/ Batch	pH = 2.5 - 3, Fe(II) = 12  mM $H_2O_2 = 0.045 \text{ g g}^{-1} \text{ soil}$ 28%  of diesel was degra with soil minerals (withouthouthouthouthouthouthouthouthouthou		(Villa et al., 2010)
H <sub>2</sub> O <sub>2</sub>	Soluble Fe(III) with EDTA	Petroleum hydrocarbons Dichloromethane- extractable organics 14.8 g Kg <sup>-1</sup>	Soil samples collected from areas adjacent to oil wells/ Batch	pH = 7, $H_2O_2$ = 2.45 mol Kg <sup>-1</sup> soil, $H_2O_2$ :Fe(III) molar ratio = 200:1.	>80% removal of hydrocarbons	(Lu et al., 2010)
$Na_2S_2O_8$	Soluble Fe(II)	Diesel 5 g Kg <sup>−1</sup>	Spiked sand and soil/ Batch	pH = 3, Oxidant:Fe molar ratio = 100:1	38% removal but inclusion of metal oxides improved the oxidation efficiency	(Do et al., 2010)
$Na_2S_2O_8$	Soluble Fe(II)	Diesel TPH = 3.5 g Kg⁻¹	Soil from an oil refining plant/Batch	Oxidant = 20% Oxidant:Fe = 1:0.01	Total removal 40% after 60 days, Reaction rate constant = $1.47 \times 10^{-2} \text{ day}^{-1}$	(Yen et al., 2011)
$H_2O_2$ or $Na_2S_2O_8$	Soluble Fe(II) Or Magnetite (lab synthesized)	Petroleum hydrocarbons 4 g Kg <sup>-1</sup> of crude and weathered oil	Spiked sand/ Batch	pH = 6.7, 20 - 25  °C, magnetite = 10% w/w, oxidant:Fe molar ratio = 10:1 (H <sub>2</sub> O <sub>2</sub> ) and 1:1	80-90% of hydrocarbon removal by both oxidants in the presence of magnetite after one week. <10 % of	(Usman et al., 2012a)

	30 nm; 103 m <sup>2</sup> g <sup>-1</sup>			$(Na_2S_2O_8)$	pollutant removal with soluble Fe(II) as catalyst	
$H_2O_2$ or $Na_2S_2O_8$	Magnetite (lab synthesized) 30 nm; 103 m <sup>2</sup> g <sup>-1</sup>	Petroleum hydrocarbons 4 g Kg <sup>-1</sup> of weathered oil	Spiked sand/ Saturated column	pH = 6.7, 20 - 25  °C, magnetite = 10% w/w, oxidant:Fe molar ratio = 10:1 (H <sub>2</sub> O <sub>2</sub> ) and 1:1 (Na <sub>2</sub> S <sub>2</sub> O <sub>8</sub> )	60-70% of hydrocarbon removal by both oxidants	(Usman et al., 2013)
H <sub>2</sub> O <sub>2</sub>	Soluble Fe(III) with or without chelating agent	Biodiesel blend (20 % biodiesel, 80 % diesel) TPH = 1 g Kg <sup>-1</sup>	Spiked sandy clay loam/ Batch	pH = < 3 (without chelating agent) and 4.5 - 6 (with chelating agent) Fe (III) = 20 mM, Citrate = 50 mM, $H_2O_2 = 4000 \text{ mM}$ Fightharpoint for the second secon		(Pardo et al., 2014)
$H_2O_2$	Magnetite and ZVI	Diesel TPH = 5 g Kg <sup>-1</sup>	Spiked soil/ Batch	pH = 6.7-7.4 Catalyst = 4.27 wt% $H_2O_2 = 2.17 \text{ mol L}^{-1}$	TPH removal was 57% (magnetite) and 67% (ZVI)	(Jamialahma di et al., 2015)
H <sub>2</sub> O <sub>2</sub>	Soluble Fe(II) with chelating agent	Crude oil TPH = 15.2 and 27.7 g $Kg^{-1}$	Soils collected from two oil wells / Batch	pH = 7.5, Fe(II) = 5.8 mM, H <sub>2</sub> O <sub>2</sub> = 1100 mM Citric acid = 17.9 g L <sup>-1</sup>	40-50% of TPH removal	(Xu et al., 2016b)
$H_2O_2$	Soluble Fe(II) with chelating agent	Crude oil contamination TPH = $23.4 \text{ g Kg}^{-1}$	Soil collected from an oil well/ Batch	$ \begin{array}{l} pH = 6.5 - 7, \\ Fe(II) = 2.9 \text{ mM}, \\ H_2O_2 = 900 \text{ mM} \end{array} > 20\% \text{ removal of} \\ hydrocarbons in 10 days \end{array} $		(Xu et al., 2017)
$Na_2S_2O_8$	NaOH	Diesel TPH = 4.9 g Kg <sup>-1</sup>	Soil collected from train maintenance facility/Batch	$pH = \ge 12, 20 \text{ °C},$ $Na_2S_2O_8 = 420 \text{ mM},$ $NaOH:Na_2S_2O_8 = 4,$ Liquid/solid = 2 mL g <sup>-1</sup>	98% removal of TPH after 56 days.	(Lominchar et al., 2018)

**Table 1:** Summary of studies using chemical oxidation to remove oil hydrocarbons in contaminated soils.

#### 104 **2. Experimental section**

#### 105 **2.1. Chemical reagents and materials**

Following reagents were used: FeSO<sub>4</sub>.7H<sub>2</sub>O with purity greater than 98% obtained from
VWR, sodium persulfate (Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>) and hydrogen peroxide 35% (H<sub>2</sub>O<sub>2</sub>) of Acros Organics.
Dichloromethane and chloroform, both purchased from VWR were used as received.
Deionized water was produced with a Milli–Q system from Millipore.

- 110 Magnetite used in the present study was synthesized and characterized in the context of 111 previous study (Usman et al., 2012a). This magnetite is characterized as nano-magnetite 112 (particle size range of 30 - 50 nm) with BET surface area of  $103 \pm 2$  m<sup>2</sup> g<sup>-1</sup>, PZC of 7.9 and
- 113 Fe(II)/Fe(III) ratio of 0.46.

#### 114 **2.2. Sediment samples**

115 This study concerned three contaminated sediments from two different harbors, and one petroleum industrial channel. The locations of these three sites are shown in the Figure 1 and 116 117 are detailed below: LGH Sediments were sampled in February 2007 by dredging in Le 118 Guilvinec harbor (north-western of France), TMH Sediments were dredged in Toulon 119 military harbor (southern France) in April 2008, PIC sediments were sampled in 2011 in a 120 petroleum industrial channel located in the south of France. These samples were freeze-dried, 121 sieved at 2 mm, placed in glass bottles, and stored at 5 °C before analysis and/or treatment. 122 Properties of the tested sediments are reported in Table 2.

- 123 These three locations are affected by petroleum by-product contamination for several decades
- 124 and polluted sediments have already undergone natural biological alteration.



126 **Figure 1:** Location of tested sediments in France

127

#### 128 **2.3. Oxidation procedures**

129 Following experiments were performed to evaluate the chemical oxidation of contaminated 130 sediments: H<sub>2</sub>O<sub>2</sub> alone, H<sub>2</sub>O<sub>2</sub>/Fe(II), H<sub>2</sub>O<sub>2</sub>/magnetite, Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub> alone, Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/Fe(II), and 131 Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/magnetite. Experiments were performed in batch slurry without pH adjustment (circumneutral), room temperature (20 - 25 °C), in the absence of light (by aluminum foil 132 133 coverings). Oxidant dose was adjusted according to the oxidant:Fe molar ratio equal to 20:1 134  $(H_2O_2)$  and 2:1 (Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>) in slurry on the basis of our previous studies (Usman et al., 2012a; 135 2012b). Because the parasite reactions including nonproductive oxidant demand and 136 hydroxyl radical scavenging are more important for H<sub>2</sub>O<sub>2</sub> (Liang et al., 2004; Xue et al., 137 2009b; Usman et al., 2012a; 2012b), we used higher dose of H<sub>2</sub>O<sub>2</sub> than persulfate. Blank 138 experiments were performed by using magnetite alone without any oxidant but no pollutant 139 degradation was observed (data not shown). Magnetite was added in concerned sediments to

140 achieve 10% w/w as final contents (0.1 g of magnetite for 1 g of sediment). Equivalent molar 141 amount of Fe was used to compare the efficiency of both catalysts (soluble Fe(II) and magnetite) to activate the tested oxidants. Standard procedure is detailed in our previous 142 143 study by Usman et al. (2012a). Sediments (2 g) were stirred for 15 minutes with suitable 144 amount of water to have a final volume of 20 mL after oxidant addition. Photocatalytic 145 degradation was avoided by using aluminum foil coverings. Theses slurries were reacted for 146 one week under vigorous magnetic-stirring. Reaction was then stopped by freezing these 147 batches. After two days, water was removed by freeze drying these samples.

One week time point was chosen based on previous studies where no further degradation was observed after one week (Usman et al., 2012a; 2012b) while oxidants were fully consumed after this period as confirmed by iodometric titration (Rybnikova et al., 2016). All experiments were performed in duplicates and results are expressed as a mean value of the 2 experiments and standard deviation of the duplicates was less than 5%.

#### 153 **2.4. Extraction and analysis**

154 Quantification of extractable organic matter (EOM): Freeze-dried sediments were extracted 155 with chloroform at 60 °C for 45 min as detailed previously (Usman et al., 2016a). This was performed in a glass vessel which was connected to a water-cooled reflux condenser to let 156 157 reflux the evaporated solvent. Temperature of extraction medium was homogenized by 158 magnetic stirring. After extraction, the vessel was allowed to cool at room temperature before 159 opening it. The supernatant was filtered through a pre-washed glass microfiber filter (d = 45160 mm, porosity = 0.7 mm; Whatman). Volume of organic extract was reduced to 20 mL under 161 N<sub>2</sub> and 5 mL of this solution was transferred in a pre-weighed vial. The amount of extractable organic matter (EOM) was determined by weighing the vial after evaporation of the solvent. 162 163 This method resulted in complete recovery of EOM in previous studies (Usman et al., 2012a; 164 2012c).

165 Hydrocarbon Index (HI) quantification: The HI was measured according to the ISO 166 16703:2004 procedure using a GC-FID 7890 Agilent technologies. Briefly, a standard 167 mixture (ASTM D5307) is used to define the integration limits of the chromatogram area. These limits correspond to the *n*-decane ( $C_{10}H_{22}$ ) and *n*-tetracontane ( $C_{40}H_{82}$ ) retention time. 168 169 An ISO 11046 standardized oil is used as standard solution (external calibration). Seven solutions of different concentrations (0.5, 1, 2, 4, 6, 8 and 10 mg mL<sup>-1</sup>) are prepared from this 170 171 standardized oil solution and injected into the chromatograph in order to obtain calibration 172 curves. The integration of the area under each chromatogram is corrected by the background noise (by integrating the area chromatogram obtained with a sample of pure dichloromethane 173 174 that serves as a control).

#### 175 **3. Results and discussion**

#### 176 **3.1. Characterization of sampled sediments**

177 The main properties of tested sediments are reported in Table 2. These sediments were 178 characterized by different mineral fractions including sand (LGH, 98% sand), silt loam (TMH, 35% sand, 57% silt), and silt (PIC, 9% sand, 81% silt, 10% clay) with different pH 179 180 values: 8.60 (LGH), 8.28 (TMH) and 7.67 (PIC). Total organic carbon (TOC) contents were 181 in order of 1.85%, 4.96% and 8.39% in LGS, TMH and PIC sediments, respectively. 182 Observed order of TOC contents could be correlated to increasing silt contents and decreasing sand contents as reported by Augustin and Cihacek (2016). Indeed, total silt was 183 184 positively correlated ( $P \le 0.01$ ) to the TOC while sand was negatively correlated ( $P \le 0.10$ ) to it. An order similar to TOC was observed for HI values: LGH (3.7 g kg<sup>-1</sup>) < TMH (5.5 g 185  $kg^{-1}$ ) < PIC (9.0 g  $kg^{-1}$ ). These sediments contained higher CaCO<sub>3</sub> amounts of 18.63% 186 187 (LGH), 28.43 (TMH) and 23.1 (PIC). Higher content of Cu, Pb and Zn were also detected in 188 these sediments (Table 2).

189 The molecular distributions of initial sediments (Figure 2) are dominated by UCM which 190 comprise a mixture of iso- and cyclo-alkanes (Tolosa et al., 2004) and cannot be resolved by 191 classical chromatographic column. The main identified products correspond to pentacyclic 192 triterpanes. Such signatures are typical of biodegraded and weathered oil containing 193 compounds which are resistant to biodegradation (Tolosa et al., 2004; Farrington and Quinn, 194 2015). Sampled areas were under natural attenuation for years which eliminated the easily 195 biodegradable *n*-alkanes leaving UCM as the sole contamination in three sediments. GC-FID 196 chromatograms (Fig. 2) provide a visual representation of efficiency of chemical oxidation to 197 degrade UCM as observed previously in spiked sand (Usman et al., 2012a).

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	LGH	ТМН	PIC
Origin of sediments	Le Guilvinec harbor	Toulon military harbor	Petroleum industrial channel
Granulometric fraction	0-1 mm	0-1 mm	0-2 mm
Clay (<2 µm) (g kg⁻¹)		75	100
Fine silt (2–20 $\mu$ m) (g kg <sup>-1</sup> )	15*	376	440
Coarse silt (20–50 $\mu$ m) (g kg <sup>-1</sup> )		196	370
Fine sand (50–200 $\mu$ m) (g kg <sup>-1</sup> )	215	266	90
Coarse sand (200–2000 $\mu$ m) (g kg <sup>-1</sup> )	772	87	0
nH (water)	8 60	8 28	7 67
	19.62	29.42	22.1
	10.03	28.43	23.1
	1.85	4.96	8.39
HI (g kg <sup>-1</sup> )	3.7	5.5	9.0
Total element contents			
Fe (g kg <sup>-1</sup> )	15.39	30.00	110.29
P (g kg <sup>-1</sup> )	2.12	0.56	9.4
K (g kg <sup>-1</sup> )	5.87	7.69	1
Mg (g kg <sup>-1</sup> )	7.22	14.36	8.9
Ca (g kg <sup>-1</sup> )	67.15	109.77	144.9
Na (g kg <sup>-1</sup> )	2.37	17.08	5.3
As (mg kg <sup>-1</sup> )	N.D.	125.95	46.9
Cd (mg kg <sup>-1</sup> )	N.D.	N.D.	1.9
Cr (mg kg <sup>-1</sup> )	82.36	71.08	135
Cu (mg kg <sup>-1</sup> )	659.65	1498.76	83.7
Hg (mg kg <sup>-1</sup> )	N.D.	59.31	0.5
Ni (mg kg <sup>-1</sup> )	26.13	29.27	43.4
Pb (mg kg <sup>-1</sup> )	364.94	597.52	66.7
Zn (mg kg <sup>-1</sup> )	588.28	1760.74	802

**Table 2:** Salient characteristics of tested sediments

202 \* represents the sum of clay, fine silt and coarse silt.



204 UCM : Unresolved Complex Mixture

Figure 2: GC-FID spectra of tested sediments before (initial) and after chemical oxidation by H<sub>2</sub>O<sub>2</sub>/magnetite and Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/magnetite. Tested sediments were obtained from Le Guilvinec harbor (LGH), Toulon military harbor (TMH) and petroleum industrial channel (PIC). Each organic extract was analyzed by GC-FID using the same procedure (same initial amount of soil before treatment, same amount of solvent for the extraction of sediment after treatment and same volume injected in the GC-FID).

#### 211 **3.2** Chemical oxidation of contaminated sediments

212 Contaminated sediments were subjected to chemical oxidation in batch experiments. 213 Efficiency of various oxidation treatments was tested at circumneutral pH including  $H_2O_2$ 214 alone,  $H_2O_2/Fe(II)$ ,  $H_2O_2/magnetite$ ,  $Na_2S_2O_8$  alone,  $Na_2S_2O_8/Fe(II)$ , and  $Na_2S_2O_8/magnetite$ . 215 Evolution of extractable organic matter (EOM) was obtained by measuring the weight of 216 organic extract before and after chemical oxidation (Figure 3).



Figure 3: Extractable organic matter (EOM) before (T0) and after chemical oxidation by H<sub>2</sub>O<sub>2</sub>/magnetite (A) and Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/magnetite (B) in contaminated sediments obtained from Le Guilvinec harbor (LGH), Toulon military harbor (TMH) and petroleum industrial channel (PIC). Experimental conditions were sediment = 2 g, volume of solution = 20 mL, oxidant doses were used according to the oxidant:Fe molar ratio equal to 20:1 (H<sub>2</sub>O<sub>2</sub>) and 2:1 (Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>) with 10% w/w magnetite.

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Obtained results (Figure 3) indicated a significant decrease in EOM (25 – 50%) when magnetite was used as a catalyst. In TMH, EOM removal extent was lowest (~25% by both oxidants) that might be correlated to its higher carbonate contents (28.43% in TMH sediments as compare to the 18.63% and 23.1% in LGH and PIC sediments, respectively). Carbonates were shown to have scavenging effects for radicals and thus resulting in 230 decreased oxidation efficiency (Liang et al., 2006; Grebel et al., 2010). Loss of EOM was 231 50% and 32% in LGH sediments and 48% and 35% in PIC sediment by H<sub>2</sub>O<sub>2</sub>/magnetite and 232 Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/magnetite, respectively. However, use of both oxidants alone or with soluble Fe(II) 233 resulted in lower removal of EOM (< 5 %, data not shown) that can be associated to the 234 inability of Fe(II) to catalyze chemical oxidation at circumneutral pH (Xue et al., 2009b; 235 Usman et al., 2012a). Soluble Fe(II) precipitates at circumneutral pH which obstructed its catalytic ability. Reaction pH is very important factor controlling the remediation efficiency. 236 237 Owing to its strong stability, magnetite was found effective at a wide range of pH (Usman et 238 al., 2016b).

239 Hydrocarbon index (HI) measured by GC-FID is presented in Figure 4. Use of magnetitecatalyzed chemical oxidation resulted in approximately 30 - 70% removal of oil 240 hydrocarbons in tested sediments. On the other hand, negligible degradation (< 5%) was 241 242 observed when both oxidants were applied alone or with soluble Fe(II) (data not shown). Xu et al. (2017) also reported a comparable oxidation efficiency by  $H_2O_2$  in the presence or 243 absence of Fe(II) at circumneutral pH (6.5 - 7) in loamy soil highlighting the inability of 244 245 Fe(II) to act as a catalyst. They observed that use of  $H_2O_2$  (225, 450 and 900 mM) with 246 soluble Fe(II) (2.9 mM) resulted in total petroleum hydrocarbon removal of 2, 15, and 25%, respectively whereas a comparable oxidation efficiency was noted by  $H_2O_2$  without Fe(II) of 247 1, 17, and 22%, respectively (Xu et al., 2017). It should, however, be noted that total 248 concentration of native Fe(II) in their soil was 4.8 g kg<sup>-1</sup> which could explain the reported 249 250 oxidation efficiency without any added Fe(II) by Xu et al (2017). Native Fe in contaminated soils has been found to catalyze Fenton-like oxidation with no Fe addition for the removal of 251 PAHs in contaminated soils with 57.5 g kg<sup>-1</sup> endogenous Fe oxides (amorphous + crystalline) 252 253 (Watts et al., 2002). Similary, Flotron et al. (2005) reported an equivalent PAH degradation by H<sub>2</sub>O<sub>2</sub>/soluble Fe(II) and H<sub>2</sub>O<sub>2</sub> in contaminated sludge (pH 8.8) and sediments (pH 4.4) 254

bearing 94 and 30 g kg<sup>-1</sup> as total native Fe, respectively. Owing to the presence of native Fe 255 (16.4 g kg<sup>-1</sup>), 52% of PAHs were degraded by  $H_2O_2$  (0.4 g g<sup>-1</sup> soil) under saturated 256 conditions without any Fe(II) addition (Palmroth et al., 2006). Role of endogenous Fe (18.2 g 257 kg<sup>-1</sup>) was also highlighted by Pardo et al. (2016) when they observed similar degradation of 258 PAHs by Fenton oxidation (882 mM H<sub>2</sub>O<sub>2</sub> without pH adjustment) by adding 259 1 mM Fe(III) or without external addition of Fe. However, Usman et al. (2012b; 2012c) 260 reported that native iron (25 g kg<sup>-1</sup> Fe<sub>2</sub>O<sub>3</sub>) was unable to catalyze H<sub>2</sub>O<sub>2</sub> and Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub> to 261 remediate PAH contaminated soils at circumneutral pH. Similarly, Ahmad et al. (2010) 262 observed that native iron oxides (8.8 g kg<sup>-1</sup> amorphous + crystalline) in soil did not promote 263 264 measureable activation of Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub> in natural soils. They suggested that quantities of native 265 iron oxides are not sufficient to catalyze persulfate oxidation in soils. However, even at varying concentrations of native iron  $(15 - 110 \text{ g kg}^{-1})$  in tested sediments, it was found 266 ineffective in promoting the oxidation reaction for harbor sediments. Thus, catalytic role of 267 268 native Fe oxides is variable depending on many factors including their nature, total content 269 and availability of Fe oxides.



Figure 4: Hydrocarbon index (HI) before (T0) and after chemical oxidation by H<sub>2</sub>O<sub>2</sub>/magnetite (A) and Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/magnetite (B) in contaminated sediments obtained from Le Guilvinec harbor (LGH), Toulon military harbor (TMH) and petroleum industrial channel (PIC). Experimental conditions were sediment = 2 g, volume of solution = 20 mL, oxidant doses were used according to the oxidant:Fe molar ratio equal to 20:1 (H<sub>2</sub>O<sub>2</sub>) and 2:1 (Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>) with 10% w/w magnetite.

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278 A good correlation was observed between hydrocarbon index and extractable organic matter 279 for H<sub>2</sub>O<sub>2</sub>/magnetite highlighting the non-specific nature of chemical oxidation to degrade the 280 non-target compounds. However, Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/magnetite resulted in lower removal of EOM 281 while higher loss of HI especially in the PIC sediments. It should be noted that HI quantifies 282 only low molecular weight compounds (less than 40 carbons), whereas EOM quantifies low as well as high molecular weight compounds. This observed difference in degradation of 283 284 EOM and HI by Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/magnetite could be caused by selective behavior of persulfate 285 oxidation as observed previously where it showed less efficiency towards high molecular weight PAHs while Fenton oxidation was equally efficient for all PAHs (Usman et al., 286 287 2012b; 2012c). Similarly, when crude oil rich in *n*-alkanes with pristane and phytane spiked 288 on sand was subjected to magnetite-catalyzed chemical oxidation (Usman et al., 2012a), 289  $H_2O_2$ /magnetite showed non-selective oxidation with equal efficiency towards all *n*-alkanes  $(C_{21} - C_{36})$ . On the other hand, Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/magnetite was less reactive towards high molecular 290 291 weight *n*-alkanes  $(C_{31} - C_{36})$ . However, it is difficult to point out such selectivity in studied 292 sediments because they are contaminated with UCM whereby individual components of this 293 complex mixture are difficult to resolve (Farrington and Quinn, 2015). Observed difference 294 in term of degradation of EOM and HI for persulfate for PIC sediments could also be correlated to the lower affinity of Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub> towards natural organic compounds leading to 295 296 higher removal of target pollutants (Lim et al., 2016). Very recently, non-productive 297 consumption of Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub> was lower than 10% after 56 days of reaction in non-polluted soil (despite 6.5% CaCO<sub>3</sub>) highlighting the low reactivity of oxidant with different soil 298

components (Lominchar et al., 2018). Rather, persulfate was also found to be activated at basic pH by organic compounds similar to those present in soil organic matter (Ahmad et al., 2010). Similarly, the impact of soil matrix was less pronounced on the efficiency of persulfate oxidation to remove PAHs from historically contaminated soil as compared to the Fenton oxidation system (Usman et al., 2012b; 2012c).

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#### 305 **3.3 Magnetite-catalyzed chemical oxidation** *vs.* **common oxidation systems**

As mentioned above, the available literature severely lacks investigations on the chemical oxidation of oil hydrocarbons in real contaminated sediments (Table 1) and thus a fair comparison of present findings with the literature is not straightforward. Previous studies were either performed on artificially contaminated sand/soil or soil obtained from contaminated site (Table 1) and present study is the first report of using magnetite-catalyzed chemical oxidation in real sediments.

Most of the remediation studies to degrade oil hydrocarbons employing H<sub>2</sub>O<sub>2</sub> and Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub> 312 313 were performed at acidic pH ( $\leq$  3) by Fe-catalyzed chemical oxidation (Kong et al., 1998; 314 Goi et al., 2006; Do et al., 2010; Villa et al., 2010; Pardo et al., 2014) (Table 1). Due to detrimental effects of this initial acidification, efforts were made to perform chemical 315 316 oxidation of oil hydrocarbons at circumneutral pH by using catalytic ability of basic oxygen 317 furnace slag (Tsai and Kao, 2009), soluble Fe(III) or Fe(II) with chelating agents (CAs) like 318 EDTA or trisodium citrate or citric acid (Lu et al., 2010; Pardo et al., 2014; Xu et al., 2016b; 319 Xu et al., 2017), magnetite (Usman et al., 2012a; 2013; Jamialahmadi et al., 2015) and zero-320 valent Fe (Jamialahmadi et al., 2015). Very high pH (>12) also resulted in strong activation 321 of Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub> for the removal of diesel. Use of chelating agents resulted in effective removal of 322 oil hydrocarbons (Table 1). However, these CAs being organic in nature will act as oxidant 323 scavenger by competing with the target pollutants (Pardo et al., 2014; Usman, 2016). For 324 example, Pardo et al. (2014) applied Fenton oxidation to treat biodiesel contaminated soil 325 with or without trisodium citrate as CA (for details of experimental conditions, see Table 1). 326 Obtained oil hydrocarbon removal reached 75% in the absence of CA (at pH <3). Use of CA 327 allowed them to perform chemical oxidation at higher pH (5-6) but degradation efficiency decreased to 37% which was associated to the consumption of oxidant by CA at higher pH. 328 329 Use of CA can also be pH sensitive as reported by Lu et al. (2010). H<sub>2</sub>O<sub>2</sub> catalyzed by Fe(III) in the presence of a CA (EDTA) was more efficient to degrade petroleum hydrocarbons at pH 330 331 7 while oxidation efficiency decreased at pH 6 which was associated to quick degradation of 332 EDTA leading to the precipitation of Fe(III). However as reported in literature, magnetite has 333 shown strong stability and catalytic capacity over a wide range of pH and thus, it offers 334 control over drawbacks associated to initial acidification or CAs. Moreover owing to its 335 ferromagnetic nature, it can be easily recovered after reaction by magnetic separation and can 336 be used for further oxidation cycles without any significant decline in catalytic ability (Xue et 337 al., 2009a; Jia et al., 2018). Other reusability studies indicated a decline in oxidation 338 efficiency of 20% after 8 oxidation cycles for the removal of phenol in aqueous solutions 339 (Zhang et al., 2009). However, reusability and/or fate of magnetite has rarely been 340 investigated in soils or sediments.

Regarding efficiency of magnetite-catalyzed chemical oxidation in present study, degradation of hydrocarbons varied between 40 - 70% when tested sediments were subjected to chemical oxidation at circumneutral pH with oxidant:Fe molar ratio equal to 20:1 (H<sub>2</sub>O<sub>2</sub>) and 2:1 (Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>) with 10% w/w magnetite. This would be economically relevant by avoiding initial acidification and/or use of chelating agents.

It is worth noting that efficiency of chemical oxidation is strongly limited by the availability
of polycyclic aromatic hydrocarbons (PAHs) in aged contaminated soils and sediments
(Flotron et al., 2005; Choi et al., 2014; Usman et al., 2016b). As a matter of fact,

349 H<sub>2</sub>O<sub>2</sub>/magnetite or Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>/magnetite did not cause any PAH degradation unless tested soils 350 were subjected to chemical (Usman et al., 2012c) or thermal pretreatment (Biache et al., 351 2015; Usman et al., 2016a). However, no such pollutant unavailability was observed for oil 352 hydrocarbons in tested sediments. It might be correlated to difference between the nature of both matrices (soils vs. sediments), history of contamination and type of pollutants (aliphatic 353 354 vs. aromatic) (Flotron et al., 2005; Trellu et al., 2017; Lominchar et al., 2018). The specific deposition, the preservation in water can probably explain the difference in term of 355 356 availability between soils and sediments. Moreover, in our case, the contamination originated 357 from petroleum source (a liquid) compared to coal-tar (source of PAHs) which becomes solid 358 with aging while losing the low molecular compounds which leads to enrichment of heavy 359 compounds in coal-tar particles (Trellu et al., 2017). Coal-tar can be observed in historically 360 contaminated soil as a small ball-like aggregate with low specific area as compared to the 361 petroleum pollution which exists as a thin film on minerals in sediments (Trellu et al., 2017). In addition to the *in-situ* application, magnetite-catalyzed chemical oxidation could offer a 362 363 quick and cost-effective alternative to conventional remediation strategies (landfilling, 364 stabilization etc.) for dredged sediments (Akcil et al., 2015) ensuring safe reuse of dredged sediments. 365

#### 366 4. Conclusion

This is the premier study reporting the use of magnetite-catalyzed chemical oxidation to remove biorefractory oil residues (remaining of natural attenuation) in different historically contaminated sediments. Magnetite showed strong efficiency to catalyze chemical oxidation at circumneutral pH. Oxidation efficiency was, however, limited by the nature and properties of sediments. No issue related to pollutant availability was observed as was the case for PAH aged contaminated soils which might be correlated to the difference of contaminant type (aliphatic hydrocarbons and PAHs) and mediums (soils and sediments). Due to the strong

- 374 efficiency of magnetite to degrade biorefractory oil residues without any initial acidification
- 375 (circumneutral pH), this study may have strong implications to design an innovative stand-
- alone technology for *in-situ* and ex-situ remediation of contaminated sediments.

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